

UNITS		Design Equations (gas phase)		Design Equations (liquid phase)	
Variables	Units	CSTR	PFR	CSTR	PFR
temperature	kelvin	$V=(F_{Ao} \cdot X)/-r_a$	$dF_a/dV=r_a$	$V=(F_{Jo}-F_j)/-r_j$	$r_j=dF_j/dV$
activation energy	joules	$F_{Ao}=C_{Ao} \cdot v_o$	$F_a=F_{Ao}(1-X)$	$V=(v_o C_{Jo}-v C_j)/-r_j$	$V=F_{Jo} \rightarrow F_j \int dF_j/r_j$
volume	$1 \text{ dm}^3 = 1 \text{ liter}$	$V=(C_{Ao} v_o X)/-r_a$	$dF_a=d(-F_{Ao}(1-X))=-F_{Ao} \cdot dX \Rightarrow F_{Ao} \cdot dX/dV=-r_a$	$V^{isom}=v_o(C_{Ao}-C_a)/k_{Ca}$	$r_a=dF_a/dV$, $F_a=V C_a$
concentration	moles/liter			$V=(F_{Ao} X)/-r_a$	$r_a=(d(v_o^* \cdot C_a))/dV$
Design Equations (liquid phase)				$V=(C_{Ao} v_o X)/(k \cdot C_a)$	$V^{first order}=C_{Ao} v_o \int_0^X \frac{1}{k C_{Ao}^* (1-X)} dX$
PBR	BR	$C_{Ao}=N_{Ao}/v_o=P_{Ao}/R \cdot T_o=(y_{Ao} P_o)/R^* T_o$	$dV=F_{Ao} \cdot (dX/-r_a)=\int_0^X \frac{F_{Ao} dX}{-r_a}$	$V=(v_o^* X)/(k(1-X))$	
$dF_j/dw=r_j'$	$dN_a/dt=r_a V$	$V=(y_{Ao} P_o v_o X)/(R T_o^* - r_a)$	$F_{Ao} (dX/-r_a)=\int_0^X \frac{F_{Ao} dX}{-r_a}$	Activation Energy $k=A e^{-E_a/RT}$ $\ln k = \ln A (-E_a/RT)$ $E_a = (R \ln(k_2/k_1))/(1/T_1-1/T_2)$	
$w=(F_{Jo}-F_j)/r_j'$	$N_{Ao} (dX/dt)=-r_a V$				
	$t=N_{Ao}^* (0 \rightarrow X) \int dX/-r_a V$				
Random Shit I need to Know			PBR		
$PV=nRT \Rightarrow n/V=C_t-o=P/RT$	$-r_a=k(C_a^2 C_b-(C_c/K_c))$		$F_{Ao}^* (dX/dw)=-r_a'$		
$C_{Jo}=y_{Jo} \cdot C_{To}$	$k_c=C_c/(C_a^2 C_b)$		$W=F_{Ao} \int_0^X \frac{dX}{-r_a'}$		
$C_a=(C_{Ao}(1-X))/(1+\epsilon X)$	$-r_a=0 @ \text{equilibrium}$				
$C_b=(C_{Ao}(\theta_b-(b/a)X))/(1+\epsilon X)$					
$C_c=(C_{Ao}(\theta_c+(c/a)X))/(1+\epsilon X)$					
$C_i=C_{i0}/(1+\epsilon X)$					
		Conversion			
		$X=X_a=\text{moles of A reacted}/\text{moles of A fed in}=(N_{Ao}-N_a)/N_{Ao}$			
		$N_a=N_{Ao}(1-X)$			
		$F_a=F_{Ao}(1-X)$			
		$C_a=C_{Ao}(1-X)$			